

Proton Computed Tomography

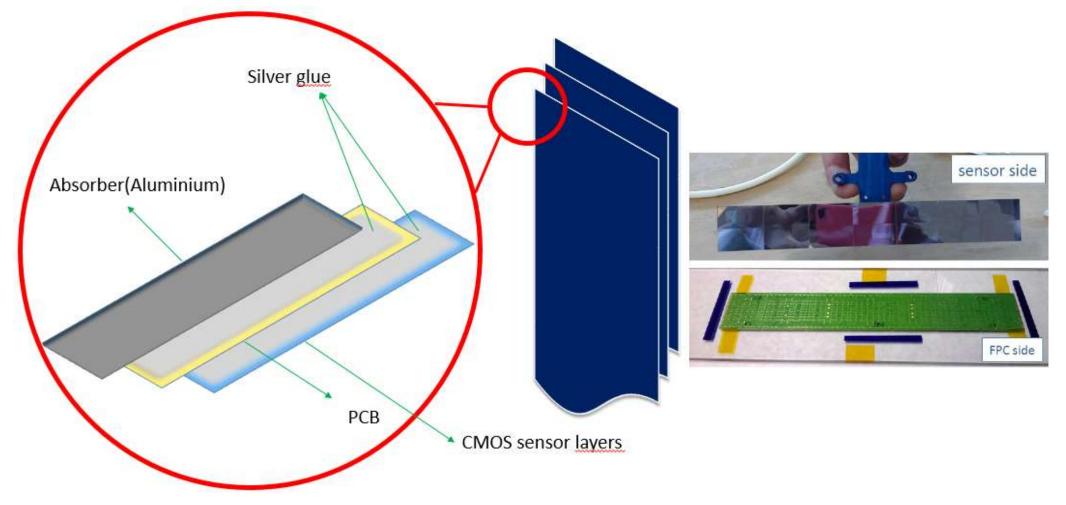
WP5, Mechanical:

Detector cooling potential, Heat transfer approach

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Potential cooling schemes



Study and simulation analysis of heat distribution field:

- In plate heat distribution
 - ✓ Geometry effect (length-width proportion)

$$q = k S \Delta T_{overall}$$

S = Shape factor

2D Geometries

Very comprehensive summary of shape factors for a large variety of geometries is given by Rohsenow and Hahne and Grigull (Heat transfer books)

3D geometries

$$S_{wall} = A/L$$

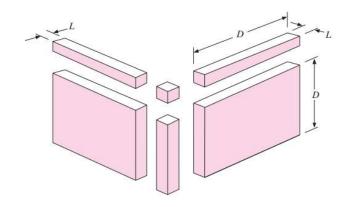
$$S_{\text{edge}} = 0.54D$$

$$S_{corner} = 0.15L$$

A = Area of wall

L = Wall thickness

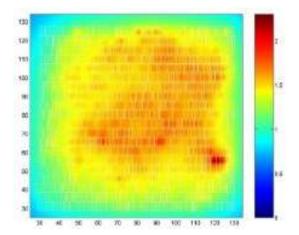
D = Length of edge



- ✓ Temperature gradient & heat transfer rate
 - a. High energy proton beams colliding location

energy gradient causes

non-uniform temperature distribution



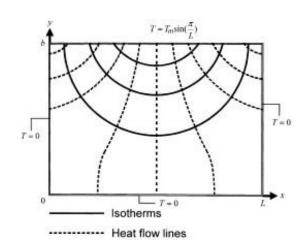
- ✓ Increasing conductivity of plate
 - a. Material/Mechanical properties of PCB, Absorber:

Higher conductivity (k)

 $\qquad \Longleftrightarrow \qquad$

Higher rate of heat transfer

- ✓ Heat spots and critical areas
- ✓ Effects of boundary conditions as cold sources



Heat transfer through stave layers

✓ Thermal conductivity of multilayer bodies(R_{Totall}):

Sensors, PCB, Silver glue, absurber

$$R=R1+R2+R3+R4+R5 = \frac{L_1}{k_1A_1} + \frac{L_2}{k_2A_2} + \frac{L_3}{k_3A_3} + \frac{L_4}{k_4A_4} + \frac{L_5}{k_5A_5}$$

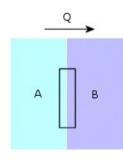


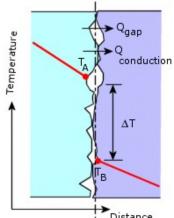


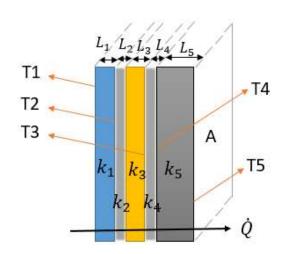
$$\dot{Q} = \frac{\Delta T}{R}$$



- $Q = \frac{Q}{R}$ Thickness layers sensitivity
- ✓ Critical layer in case of mechanical properties and heat capasity, deformation?!
- ✓ Thermal contact resistance challenge

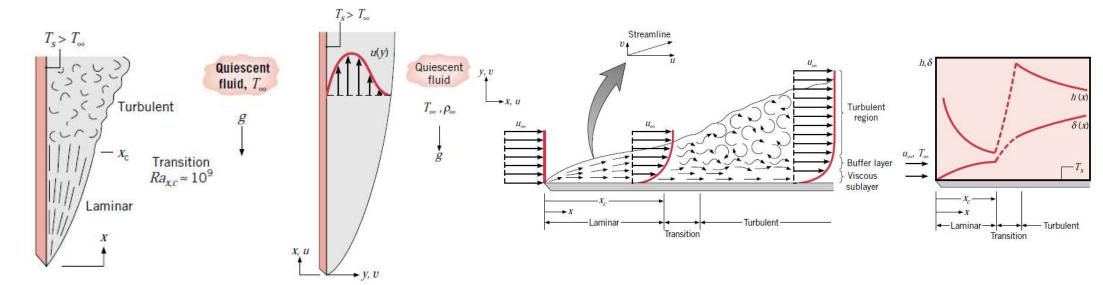






Heat transfer between staves

✓ Feasibility of air cooling convection system



- ✓ Air gap sensitivity analysis Boundary layer interaction
- ✓ Convection heat transfer rate, thermal gradient in air media between two stave
- refsers to amount of proton particle stop at previous stave and amount of particles reach to new stave? Mont Carlo?

Feasibility of various Convection heatr transfer:

- Force convection
 - Reynolds Number(Re)- ratio of inertia to viscous force-
 - Nusselt Number(Nu) Thermal Boundary layer to velocity boundary layer
- Free/Natural convection
 - b.1: Laminar Flow
 - **Bouyancy Forces**
 - Volumetric thermal expansion coeficient (β)

q= hA ΔT

Nusselt Number(Nu)

Nu=f(Gr,Pr) =
$$\frac{3}{4} \left(\frac{Gr_{\chi}}{4}\right)^{\frac{1}{4}} g(Pr)$$

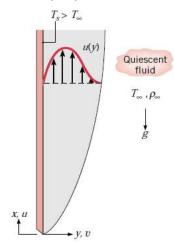
- Grashof Number (Gr)
- Prandtle Number (Pr)

b.2: Turbulence Flow

- **Bouyancy Forces**
- Volumetric thermal expansion coeficient (β)
- Nusselt Number(Nu)

Nu=f(Ra,Pr) =
$$\left\{ \left\{ 0.825 + \frac{0.387Ra^{\frac{1}{6}}}{\left[1 + \left(0.492/P_r\right)^{9/16}\right]^{8/27}} \right\}$$

- Rayleigh Number (Ra)
- Prandtle Number (Pr)
- Thermal Diffusivity (α)



- ✓ Feasibility of various Convection heatr transfer:
 - a. Force convection q= hA ΔT
 - Reynolds Number(Re)- ratio of inertia to viscous force-
 - Nusselt Number(Nu) Thermal Boundary layer to velocity boundary layer
 - Free/Natural convection

b.1: Laminar Flow

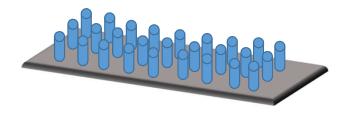
- Bouvancy Forces
- Volumetric thermal expansion coeficient (8)
- Nusselt Number(Nu)
- Nu=f(Gr,Pr) = $\frac{3}{4} \left(\frac{Gr_{\chi}}{4}\right)^{\frac{1}{4}} g(Pr)$
- Grashof Number (Gr)
- Prandtle Number (Pr) b.2: Turbulence Flow
- Bouyancy Forces
- Volumetric thermal expansion coeficient (B)
- Nusselt Number(Nu)

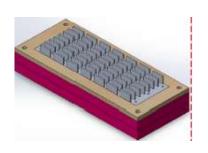
Nusselt Number(Nu)

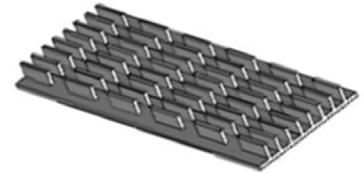
$$Nu=f(Ra,Pr) = \begin{cases} 0.825 + \frac{0.387Ra^{\frac{1}{6}}}{[1+(0.492/p_{P})^{9/10}]^{8/23}} \end{cases}$$

- Rayleigh Number (Ra)
- > Prandtle Number (Pr)
- Thermal Diffusivity (α)

- ✓ Ventilation feasibility between air gaps and sorrouding space inside calorimeter box
- ✓ Feasibility of microbodies (e.g rectangular or cylinderical) pin on absorber free side to work as heat sink to increase convection heat transfer rate







✓ Dual purpose design for calorimeter structure, with opportunity to work as support structure or stave rack/casing and also heat sink

